

## MELT PROCESSABLE COMPOSITIONS

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### Summary of the Invention

The present invention is directed to a fluoropolymer processing aid that is more efficient than conventional processing aids in eliminating melt processing problems associated with the melt processing of thermoplastic hydrocarbon polymers. In one aspect, the invention is a fluoropolymer processing aid that includes a poly(oxyalkylene) polymer and a fluoropolymer. The fluoropolymer has interpolymerized units of vinylidene fluoride and at least one other monomer wherein the vinylidene fluoride content of the fluoropolymer is greater than 65% by weight. The fluoropolymer processing aid, when blended with a thermoplastic hydrocarbon polymer to form a melt processable composition, achieves an extrudate exhibiting no melt defects at a lower level of fluoropolymer processing aid when compared to a standard processing aid system. Preferably, the content of fluoropolymer processing aid in the melt processable composition is 400 ppm or less.

In another aspect of the invention, the fluoropolymer processing aid is blended with a thermoplastic hydrocarbon polymer to form a melt processable composition. In a preferred embodiment, the fluoropolymer in the fluoropolymer processing aid is a thermoplastic copolymer having interpolymerized units of vinylidene fluoride and at least one other monomer, wherein the vinylidene fluoride content of the fluoropolymer is greater than 85% by weight. The preferred embodiment, when combined in a melt processable composition, upon extrusion achieves an extrudate exhibiting no melt defects.

The melt processable compositions of the present invention may be utilized to make items such as film, sheet, pipe, wire or cable.

For purposes of the present invention, the following terms used in this application are defined as follows:

“Polymer processing aid” means a thermoplastic or elastomeric fluoropolymer that is capable of improving polymer processing, for example, reducing melt fracture.

“Melt processable composition” means compositions or materials that are capable of withstanding processing conditions at temperatures near the melting point of at least one composition in a mixture.

“A Standard Processing Aid System” means the same components, specifically thermoplastic hydrocarbon polymer, poly(oxyalkylene) polymer, with a fluoropolymer of 60% by weight of vinylidene fluoride and 40% by weight of hexafluoropropylene and having a mooney viscosity (ML 1 + 10, 121 °C, ASTM DI646) of 36 under similar testing methods, equipment and conditions.

"Melt defects" means defects embodied in the extrudate that are generated during processing the melt processable compositions, for example melt defects may include melt fracture, die build up, chemical gel formation, or physical gel formation.

#### Detailed Description of the Invention

The compositions of the present invention reduce the melt defects encountered when melt processing polymeric materials. For purposes of the invention, melt processable polymeric materials or compositions are those that are capable of being processed while at least a portion of the composition is in a molten state. Conventionally recognized melt processing methods and equipment may be employed in processing the compositions of the present invention. Non-limiting examples of melt processing practices include extrusion, injection molding, batch mixing, and rotomolding. A preferred application of the present invention involves cast or blown film extrusion.

Melt processable compositions generally include one or more melt processable thermoplastic hydrocarbon polymers and a fluoropolymer processing aid. For purposes of the present invention, the fluoropolymer processing aid includes a fluoropolymer component and a poly(oxyalkylene) polymer.

The thermoplastic hydrocarbon polymers to which the fluoropolymer processing aid is added include conventional melt processable polymers. Most preferred are those thermoplastic hydrocarbon polymers obtained by the homopolymerization or copolymerization of olefins, as well as copolymers of one or more olefins and one or more monomers which are copolymerizable with such olefins, e.g. vinyl ester compounds such as vinyl acetate.

The preferred olefins have the general structure  $\text{CH}_2=\text{CHR}$ , where R is a hydrogen or an alkyl radical, and generally, the alkyl radical contains not more than 10 carbon atoms and preferably one to four carbon atoms. Representative olefins meeting the noted structure are fully disclosed in U.S. Patent No. 4,855,360 herein incorporated by reference in its entirety.

Preferred thermoplastic hydrocarbon polymers include polyolefins (high density polyethylene (HDPE), low density polyethylene (LDPE), linear low density polyethylene (LLDPE), polypropylene (PP), polyolefin copolymers (e.g., ethylene-butene, ethylene-octene, ethylene vinyl alcohol), or combinations thereof. Most preferred are the polyolefins.

The thermoplastic hydrocarbon polymer is generally included in the melt processable compositions in amounts of about typically greater than about 30% by weight. Those skilled in

the art recognize that the amount of polymeric binder will vary depending upon, for example, the type of polymer, the processing equipment, processing conditions and the desired end product. The thermoplastic hydrocarbon polymers may be used in the form of powders, pellets, granules, or any other extrudable form.

5           The fluoropolymer of the fluoropolymer processing aid useful in this invention are copolymers of vinylidene fluoride and at least one additional monomer, wherein the vinylidene fluoride content of the fluoropolymer is at least 65% by weight, and preferably at least 75% by weight. In a most preferred embodiment, the vinylidene fluoride content is at least 85%. At the most preferred level of vinylidene fluoride, the resulting fluoropolymer is generally considered a  
10       thermoplastic polymer.

          Non-limiting examples of monomers that may be combined with vinylidene fluoride to produce the fluoropolymer of the present invention include other fluorinated polymers, such as hexafluoropropylene, or non-fluorinated polymers, such as propylene. Preferred comonomers with vinylidene fluoride are perfluoropropylene, tetrafluoroethylene, chlorotrifluoroethylene,  
15       and pentafluoropropylene. Particularly preferred are the fluorinated polymers produced by copolymerizing perfluoropropylene and vinylidene fluoride, as described in U.S. Pat. Nos. 3,051,677 (Rexford) and 3,318,854 (Honn, et al.) and those polymers produced by copolymerizing perfluoropropylene, vinylidene fluoride and tetrafluoroethylene as described in U.S. Pat. No. 2,968,649 (Pailthorp et al.). The elastomeric copolymers of perfluoropropylene  
20       and vinylidene fluoride having between about 15 and about 50 mole percent perfluoropropylene, optionally with the addition of up to 5 to 30 mole percent tetrafluoroethylene, are particularly useful. The amount of fluoropolymer in the fluoropolymer processing aid is generally about 400 ppm or less and preferably about 200 ppm or less.

          For purposes of the invention, conventionally recognized poly(oxyalkylene) polymers  
25       may be utilized to form a component of the fluoropolymer processing aid. Poly(oxyalkylene) polymers include poly(oxyalkylene) polyols and their derivatives. U.S. Patent Nos. 4,855,360 and 5,830,947, herein incorporated by reference in their entirety, disclose various types of poly(oxyalkylene) polymers that may be suitable for use with the fluoropolymer processing aid employed in the present invention. Another examples of poly(oxyalkylene) polyols useful in  
30       this invention include those sold under the trademark Carbowax, such as Carbowax 8000 from Dow Chemical Company, Midland, MI. The amount of poly(oxyalkylene) polymer in the

fluoropolymer composition is generally added to the composition to achieve a poly(oxyalkylene) polymer to fluoropolymer ratio of 1:1 or greater.

It is generally recognized by those skilled in the art of polyolefin processing that other conventional additives may be optionally employed in melt processing application. Non-limiting examples of such additives include light stabilizers, antioxidants, antiblocking agents, slip agents, lubricants, fillers, flame retardants, foaming agents, nucleating agents, clarifying agents, colorants, coupling agents, compatibilizers, antistatic agents, antifogging agents, heat stabilizers, plasticizers, reinforcing agents, metal scavengers, acid/base scavengers, biocides or combinations thereof.

The amount of fluoropolymer processing aid present in the melt processable composition is dependent upon several variables, such as for example, the thermoplastic hydrocarbon polymer, the type of melt processing equipment, the processing conditions, and others. Those of skill in the art are capable of selecting an appropriate fluoropolymer processing aid to assist in the processing of desired thermoplastic hydrocarbon polymers. In a preferred embodiment, the fluoropolymer processing aid is used at 0.005 to 2.0% by weight of the composite. More preferably, the polymer processing aid level is between 0.01 and .05% and even more preferably between 0.02 and 0.2% by weight.

The melt processable composition of the invention can be prepared by any of a variety of ways. The addition of fluorocarbon polymer, poly(oxyalkylene) polymer, and other optional components to the thermoplastic hydrocarbon polymer can be accomplished by any of the means conveniently employed to add adjuvants to polymers. Thus the fluoropolymer and poly(oxyalkylene) polymer can be added to the hydrocarbon polymer in a Banbury mixer, or a mixing extruder. Generally, the mixing operation is carried out at a temperature above the melting point of the polymer to provide uniform distribution of the fluorocarbon polymer and poly(oxyalkylene) polymer throughout the thermoplastic hydrocarbon polymer. The fluorocarbon polymer and the poly(oxyalkylene) polymer can each be individually coated from solution onto the thermoplastic hydrocarbon polymer resin to create masterbatches of coated resin which are then dry blended with an appropriate quantity of the uncoated hydrocarbon resin to achieve the desired concentrations of fluorocarbon polymer and poly(oxyalkylene) polymer in the extrudable composition. The fluoropolymer processing additive and the host polymer may be used in the form, for example, of a powder, a pellet, or a granular product.

The resulting melt processable composition can be either extruded directly into the form of the final product shape or pelletized or otherwise comminuted into a desired particulate size or size distribution and fed to an extruder, which typically will be a single-screw extruder, that melt-processes the blended mixture to form the final product shape.

5 Melt-processing typically is performed at a temperature from 180° to 280° C, although optimum operating temperatures are selected depending upon the melting point, melt viscosity, and thermal stability of the blend. Different types of melt processing equipment, such as extruders, may be used to process the melt processable compositions of this invention. Extruders suitable for use with the present invention are described, for example, by Rauwendaal,  
10 C., "Polymer Extrusion," Hansen Publishers, p. 23-48, 1986. The die design of an extruder can vary, depending on the desired extrudate to be fabricated. For example, an annular die can be used to extrude tubing, useful in making fuel line hose, such as that described in U.S. Pat. No. 5,284,184 (Noone et al.), which description is incorporated herein by reference in its entirety.

The present invention reduces the amount of fluoropolymer processing aid required to  
15 clear melt defects when compared to a standard processing aid system. For purposes of the invention, a standard processing aid system is recognized as containing the same components, the same specifically thermoplastic hydrocarbon polymer, the same poly(oxyalkylene) polymer, with a fluoropolymer of 60% by weight of vinylidene fluoride and 40% by weight of hexafluoropropylene under the similar testing methods, equipment and conditions. The  
20 present invention achieves this significant improvement over conventionally recognized fluoropolymer processing aids. For example, the present invention, as further demonstrated in the Examples section, may clear melt defects utilizing less than 50% of the conventional fluoropolymer processing aids presently employed by industry. The present invention may preferably clear melt defects at levels of less than 200 ppm of fluoropolymer processing aid in  
25 the melt processable composition.

Although, reduction of melt defects is one mechanism to determine overall performance of the fluoropolymer processing aid, those skilled in the art understand that other processing attributes, such as for example, melt pressure, melt temperature, and mass flow rate may be positively affected through utilization of the present invention.

30 It is known in the art that a potential problem when adding fluoropolymer processing aid to polyolefins is physical and chemical gel formation. In either case, a polyolefin film having gels present can have reduced physical properties and be visually unacceptable for the product application. Therefore, it is highly desirable for a fluoropolymer processing aid to not cause gels

during processing. Physical gel formation results from using a fluoropolymer processing aid that is difficult to disperse in the polyolefin system. As a result, poorly dispersed fluoropolymer particles or gels can result. Chemical gel formation can also occur if the fluoropolymer processing aid used is thermally unstable or chemically reactive with the polyolefin resin. This can cause deleterious effects on the polyolefin resin (e.g., crosslinking) that result in chemically gelled particles being present. In either case, the presence of gelled material is unacceptable in the final extruded article (e.g. film). The fluoropolymer processing aid is capable of providing the desired performance level while exhibiting no gel formation.

The invention is further illustrated in the following examples.

## Examples

### Materials Used

Material	Description
Polyolefin 1	Exxon NTX-095, a linear low density polyethylene, commercially available from ExxonMobil, Houston, TX
Polyolefin 2	Exxon 1001.32, a linear low density polyethylene, commercially available from ExxonMobil, Houston, TX
Polyolefin 3	Exxon 1018 , a linear low density polyethylene, commercially available from ExxonMobil, Houston, TX
Polyolefin 4	Nova Surpass, a linear low density polyethylene, commercially available from Nova Chemicals, Calgary, Alberta Canada
Polyolefin 5	Exxon LV1201, a linear low density polyethylene, commercially available from ExxonMobil, Machelen, Belgium
Antiblock	Ampacet 10090, a 60 % concentrate commercially available Ampacet Corporation, Tarrytown, NY.
Slip	Ampacet 101558, a 5 % concentrate commercially available from Ampacet Corporation, Tarrytown, NY.
Slip/Antiblock Concentrate	FSU 105E , a combined slip/antiblock concentrate commercially available from A. Schulman Europe, Würselen, Germany
PEG	Carbowax 8000. A polyethylene glycol, commercially available from Dow Chemical Co., Midland, MI.
FX-5920A	Dynamar FX-5920A, a fluoropolymer based processing aid, commercially available from Dyneon LLC, Oakdale, MN.
PPA 1	Dyneon 11012, a fluoropolymer, commercially available from Dyneon LLC, Oakdale, MN.
PPA 1A	An experimental PPA containing Dyneon 11012, a fluoropolymer, commercially available from Dyneon LLC, Oakdale, MN and PEG (Carbowax 8000).
PPA 2	Dyneon 31508, a fluoropolymer, commercially available from Dyneon LLC, Oakdale, MN.
PPA 2A	An experimental PPA containing Dyneon 31508, a fluoropolymer, commercially available from Dyneon LLC, Oakdale, MN and PEG (Carbowax 8000).
PPA 3	Dyneon 1015, a fluoropolymer, commercially available from Dyneon LLC, Oakdale, MN.
PPA 3A	An experimental PPA containing Dyneon 1015, a fluoropolymer, commercially available from Dyneon LLC, Oakdale, MN and PEG (Carbowax 8000).

### Test for Determining % Melt Fracture in Polymer Films

- 5 Blown film samples were collected at 10 minute intervals during the extrusion trial. Samples were laid flat and opened along one edge with a razor blade. The sample was then placed on an overhead projector to facilitate the visual identification of the areas of the film containing melt defects. Along a line drawn on the film sample perpendicular to the direction of



the film extrusion, the widths of areas containing film defects were measured. The sum of the widths containing defects divided by the total width of the film sample gave the percent melt defects or melt fracture.

## 5 PPA Identification

The chemical compositions of the PPA formulations screened in this work are given in Table 1. These materials contained a fluoropolymer and in some cases a poly(oxyalkylene) polymer, namely Carbowax 8000.

10 **Table 1.** Identification of PPAs Examined

Example	VDF (wt %)	HFP (wt %)	CTFE (wt%)	Fluoropolymer/PEG Ratio
Dynamar FX-5920A	60	40	0	2/1
PPA 1	90	10	0	100/0
PPA 1A	90	10	0	2/1
PPA 2	85	0	15	100/0
PPA 2A	85	0	15	2/1
PPA 3	100	0	0	100/0
PPA 3A	100	0	0	2/1

### *Comparative Example 1. Melt Fracture Elimination Performance of FX-5920A*

In Comparative Example 1 a 3 % concentrate of FX-5920A in Polyolefin 1 was first made using the following procedure. Specifically, 204.3 g of Dynamar FX-5920A was dry  
 15 blended with 6.61 Kg of Polyolefin 1. The blend was compounded using a a 19 mm, 15:1 L:D, Haake Rheocord Twin Screw Extruder (commercially available from Haake Inc., Newington, NH ) equipped with a conical counter-rotating screw and a Accurate open helix dry material feeder (commercially available from Accurate Co. Whitewater, WI). The extrusion parameters were controlled and experimental data recorded using a Haake RC 9000 control data  
 20 computerized software (commercially available for Haake Inc., Newington, NH). The material was fed into the extruder at a rate of 50 g/min and was processed using the following temperature profile in each respective zone: 165 °C /190 °C /200 °C. The die was also kept at 200 °C throughout the experiment. Processing parameters (i.e., melt pressure, torque) were recorded throughout the experiment. Materials were extruded through a standard 1/8" diameter,

4-strand die (commercially available from Haake Inc., Newington, NH), water quenched, and pelletized. The sample was then re-extruded and pelletized under identical conditions to insure good PPA dispersion in the concentrate.

Films were produced using a Keifel blown film line with a 40 mm, 24/1:L/D, grooved feed extruder. The die was of spiral design, with a diameter of 40 mm and a die gap of 1.25 mm. An adjustable single lip air ring with chilled air was used for cooling. An iris and sizing cage provided further bubble stability. Film was produced with a nominal gauge of 50 microns.

The Kiefel extruder and dies zones were set at 135, 190, 220, and 210 °C respectively to maintain a melt temperature of approximately 210 °C. The screw was maintained at about 50 rpm to deliver an output of 18.2 kg/hour corresponding to a shear rate of 220 s<sup>-1</sup>.

Prior to each evaluation it was necessary to ensure that the blown film line was free of residual fluoropolymer from the previous evaluation. This was accomplished by extruding approximately 9 kg of a filled polyolefin concentrate (e.g., a 70 % CaCO<sub>3</sub> masterbatch, #HM-10, Heritage Plastics). The base resin, polyolefin 1, was then extruded for 30 minutes to insure that equilibrium processing conditions had been achieved and that the resultant film was fully melt fractured.

Samples for extrusion were prepared by weighing the required amount of fluoropolymer concentrate, pelletized resin. Comparative Example 1 was then analyzed using a minimum level protocol. In this method, the PPA level in the system was incrementally increased in a regular fashion every 60 minutes until all melt fracture is eliminated from the resultant film. In Comparative Example 1, the experiment was initially started 200 ppm of FX-5920A and incrementally increased by 200 ppm every 60 minutes until melt fracture was eliminated from the system. The level of melt fracture was analyzed as described using the aforementioned protocol. Samples were also visually analyzed for the presence of gels.

#### *Comparative Example 2. Melt Fracture Elimination Performance of FX-5920A*

Comparative Example 2 was performed in an identical fashion to Comparative Example 1 with the following exceptions. Polyolefin 2 was utilized in place of Polyolefin 1. About 1500 ppm slip and 7500 ppm antiblock were added to the formulation. The blown film die gap was changed to 0.6 mm. The film produced with a nominal gauge of 25 microns. The extruder and dies zones were set at 210, 230, 235, and 230 °C respectively to maintain a melt temperature of approximately 215 °C. The screw was maintained at about 30 rpm to deliver an output of 11.8 kg/hour corresponding to a shear rate of 520 s<sup>-1</sup>.

*Comparative Example 3. Melt Fracture Elimination Performance of FX-5920A*

Comparative Example 3 was performed in an identical fashion to Comparative Example 1 with the following exceptions. Polyolefin 3 was utilized in place of Polyolefin 1 and 1500 ppm slip and 7500 ppm antiblock were added to the formulation.

*Comparative Example 4. Melt Fracture Elimination Performance of FX-5920A*

Comparative Example 4 was performed in an identical fashion to Comparative Example 1 with the following exceptions. Polyolefin 4 was utilized in place of Polyolefin 1. About 1500 ppm slip and 7500 ppm antiblock were added to the formulation. The blown film die gap was changed to 0.6 mm. The film produced with a nominal gauge of 25 microns. The extruder and dies zones were set at 205, 215, 235, and 210 °C respectively to maintain a melt temperature of approximately 210 °C. The screw was maintained at about 15 rpm to deliver an output of 6.8 kg/hour corresponding to a shear rate of 300 s<sup>-1</sup>.

*Comparative Example 5. Melt Fracture Elimination Performance of PPA 1*

Comparative Example 5 was performed in an identical fashion to Comparative Example 3 with the exception that PPA 1 was utilized in place of FX-5920A.

*Comparative Example 6. Melt Fracture Elimination Performance of FX-5920A*

Comparative Example 6 was performed in an identical fashion to Comparative Example 1 with the following exceptions. Polyolefin 5 was utilized in place of Polyolefin 1. To the formulation was added 2 % of a commercial slip/antiblock combined concentrate (commercially available from A. Schulman). A lab scale Collin blown film line was utilized having a 45 mm extruder, 25/1:L/D, and dual lip air ring. The blown film die gap was changed to 0.6 mm. The film produced with a nominal gauge of 25 microns. The extruder and dies zones were set at 205, 205, 210, 220 and 205 °C respectively to maintain a melt temperature of approximately 210 °C. The screw was maintained at about 46 rpm to deliver an output of 11.0 kg/hour corresponding to a shear rate of 430 s<sup>-1</sup>.

*Comparative Example 7. Melt Fracture Elimination Performance of PPA 3.*

Comparative Example 7 was performed in an identical fashion to Comparative Example 3 with the exception that PPA 3 was utilized in place of FX-5920A.

*Comparative Example 8. Melt Fracture Elimination Performance of PPA 3A.*

Comparative Example 8 was performed in an identical fashion to Comparative Example 3 with the exception that PPA 3A was utilized in place of FX-5920A.

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*Example 1. Melt Fracture Elimination Performance of PPA 1A*

Example 1 was performed in an identical fashion to Comparative Example 1 with the exception that PPA 1A was utilized in place of FX-5920A.

10 *Example 2. Melt Fracture Elimination Performance of PPA 1A*

Example 2 was performed in an identical fashion to Comparative Example 2 with the exception that PPA 1A was utilized in place of FX-5920A.

*Example 3. Melt Fracture Elimination Performance of PPA 1A*

15 Example 3 was performed in an identical fashion to Comparative Example 3 with the exception that PPA 1A was utilized in place of FX-5920A.

*Example 4. Melt Fracture Elimination Performance of PPA 1A*

20 Example 4 was performed in an identical fashion to Comparative Example 4 with the exception that PPA 1A was utilized in place of FX-5920A.

*Example 5. Melt Fracture Elimination Performance of PPA 1A*

Example 5 was performed in an identical fashion to Comparative Example 6 with the exception that PPA 1A was utilized in place of FX-5920A.

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**Table 2.** Overall PPA Level Required to Eliminate Melt Fracture for Comparative Examples 1-5 and Examples 1-4.

Example	PPA	Resin Host	PPA Level Required to Clear Melt Fracture (PPM)	Gel Present
CE 1	FX-5920A	Polyolefin 1	1600	No
CE 2	FX-5920A	Polyolefin 2	1000	No
CE 3	FX-5920A	Polyolefin 3	1600	No
CE 4	FX-5920A	Polyolefin 4	800	No
CE 5	PPA 1	Polyolefin 3	>1000	No
CE 6	FX-5920A	Polyolefin 5	800	No
CE 7	PPA 3	Polyolefin 4	400	Yes
CE 8	PPA 3A	Polyolefin 4	400	Yes
Ex 1	PPA 1A	Polyolefin 1	700	No
Ex 2	PPA 1A	Polyolefin 2	400	No
Ex 3	PPA 1A	Polyolefin 3	400	No
Ex 4	PPA 1A	Polyolefin 4	400	No
Ex 5	PPA 1A	Polyolefin 5	400	No

Table 2 demonstrates that when compared to a standard fluoropolymer processing additive (FX-5920A) in a wide variety of host resins (CE 1-5) and to a high VDF copolymer that does not contain PEG (PPA 1), a greatly reduced amount of high VDF copolymers that contain PEG (PPA 1A) is required to eliminate melt fracture in the films produced. Additionally, Table 2 shows that VDF homopolymers with and without PEG (PPA 3 and 3A) suffer from the presence of gels in the resultant film whereas, the standard fluoropolymer processing additive (FX-5920A), PPA 1 and PPA 1A do not.

*Comparative Example 9. Melt Fracture Elimination Performance of FX-5920A*

Comparative Example 9 was performed in an identical fashion to Comparative Example 3 with the following exceptions. PPA 2 was utilized in place of FX-5920A.

*Example 6. Melt Fracture Elimination Performance of FX-5920A*

Example 6 was performed in an identical fashion to Comparative Example 9 with the following exceptions. PPA 2A was utilized in place of PPA 2.

**Table 3.** Overall PPA Level Required to Eliminate Melt Fracture for Comparative Example 9 and Example 6.

<b>Example</b>	<b>PPA</b>	<b>Resin Host</b>	<b>PPA Level Required to Clear Melt Fracture (PPM)</b>	<b>Gels Present</b>
CE 9	PPA 2	Polyolefin 3	>1600	No
Ex 6	PPA 2A	Polyolefin 3	1200	No

From the above disclosure of the general principles of the present invention and the preceding detailed description, those skilled in this art will readily comprehend the various modifications to which the present invention is susceptible. Therefore, the scope of the invention should be limited only by the following claims and equivalents thereof.